


<b>PROJECT :</b>			<b>DATE :</b>	
<b>PROJ. NO.:</b>			<b>BY :</b>	S.Rahimi
<b>CLIENT :</b>			<b>REV :</b>	
<b>UNIT :</b>			<b>DOC NO.:</b>	

### Two Phase PSV Sizing - $\omega$ Method (One-point Method)

Input Data		
PSV Tag No.		
P&ID No.		
Protected Equipment		
Cause of Overpressure		
Vapor Mass Flow Rate	kg/hr	35240
Liquid Mass Flow Rate	kg/hr	64760
Vapor Mass Density @ Relieving Condition	kg/m <sup>3</sup>	51.76
Liquid Mass Density @ Relieving Condition	kg/m <sup>3</sup>	457.4
Latent Heat of Vaporization	kJ/kg	238.4
Liquid Specific Heat	kJ/kgK	3.066

Operating Condition		
Maximum Operating Pressure	barg	18.00
Maximum Operating Temperature	°C	45.00
Max. Allowable Working Pressure	barg	15.00

Relieving Condition		
Set Pressure	barg	22.00
Allowable Over Pressure	%	10.0
Superimposed Back Pressure (Constant)	barg	1.00
Superimposed Back Pressure (Variable)	barg	0.00
Built Up Back Pressure	barg	0.00
Relieving Temperature	°C	155

Calculation Results		
Recommended Type (Conv./Bellows/Pilot)	<b>CONVENTIONAL</b>	
Required Relieving Capacity	kg/hr	<b>100000</b>
Vapor Mass Fraction	----	<b>0.3524</b>
Relieving Pressure	barg	<b>24.20</b>
Total Back Pressure	barg	<b>1.00</b>
$\omega$	----	<b>2.90</b>
Discharge Effective Coefficient (Kd)	----	<b>0.85</b>
Back Pressure Coefficient (Kb)	----	<b>1.00</b>
Critical Pressure	bara	<b>18.51</b>
Flow Regime	----	<b>Critical</b>
Two Phase Mass Flux	kg/m <sup>2</sup> .sec	<b>7547</b>
Calculated Orifice Area	mm <sup>2</sup>	<b>4330.1</b>
Selected Orifice Area	mm <sup>2</sup>	<b>7129.0</b>
Orifice Designation	----	<b>Q</b>
No. of Required PSVs	----	<b>1</b>
Inlet Size	in	<b>6</b>
Outlet Size	in	<b>8</b>

General Notes